



Safety Instrumented System

A Critical Barrier

Presented by:

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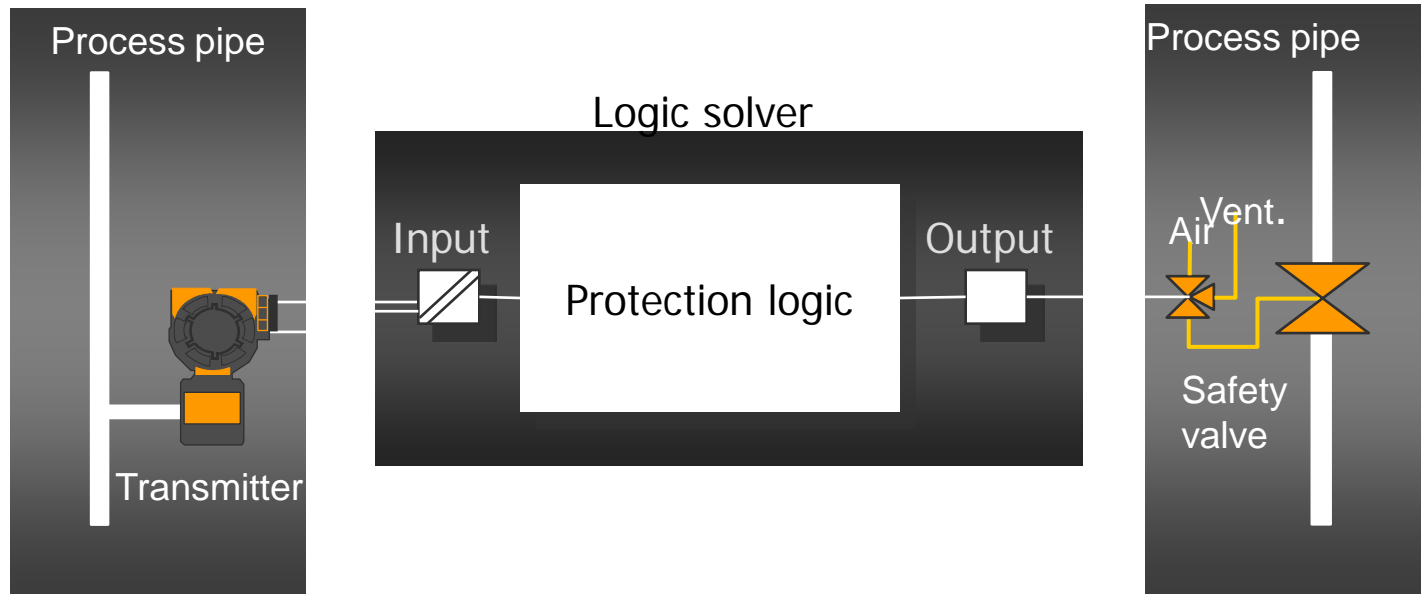
- ❖ The Safety Instrumented System
- ❖ A review of Chemical Industry Accidents
- ❖ Evolution of Regulations and Standards
- ❖ Preventing Accidents: Risk Reduction
- ❖ Concept of risk reduction
- ❖ Accidents and Causes: The Human Factor
- ❖ Safety Instrumented Systems as a safety barrier
- ❖ Design & Engineering SIS: IEC 61508/ 61511 & FSM
- ❖ Operation & Maintenance
- ❖ Safety Lifecycle expectation & expectations on users

The Safety Instrumented System

What is a Safety Instrumented System ???

A **Safety Instrumented System** is a system that provides an **independent** and **predetermined** emergency shutdown path in case a **process runs out of control**

Safety System – “IPS”, “ESD”, “SGS” etc... = **SIS**



❖ SIS: The need for Protection

EUC = Equipment Under Control

Industrial Process



Control



If something runs out of control a dangerous situation can arise ==> a **demand** for a protective action

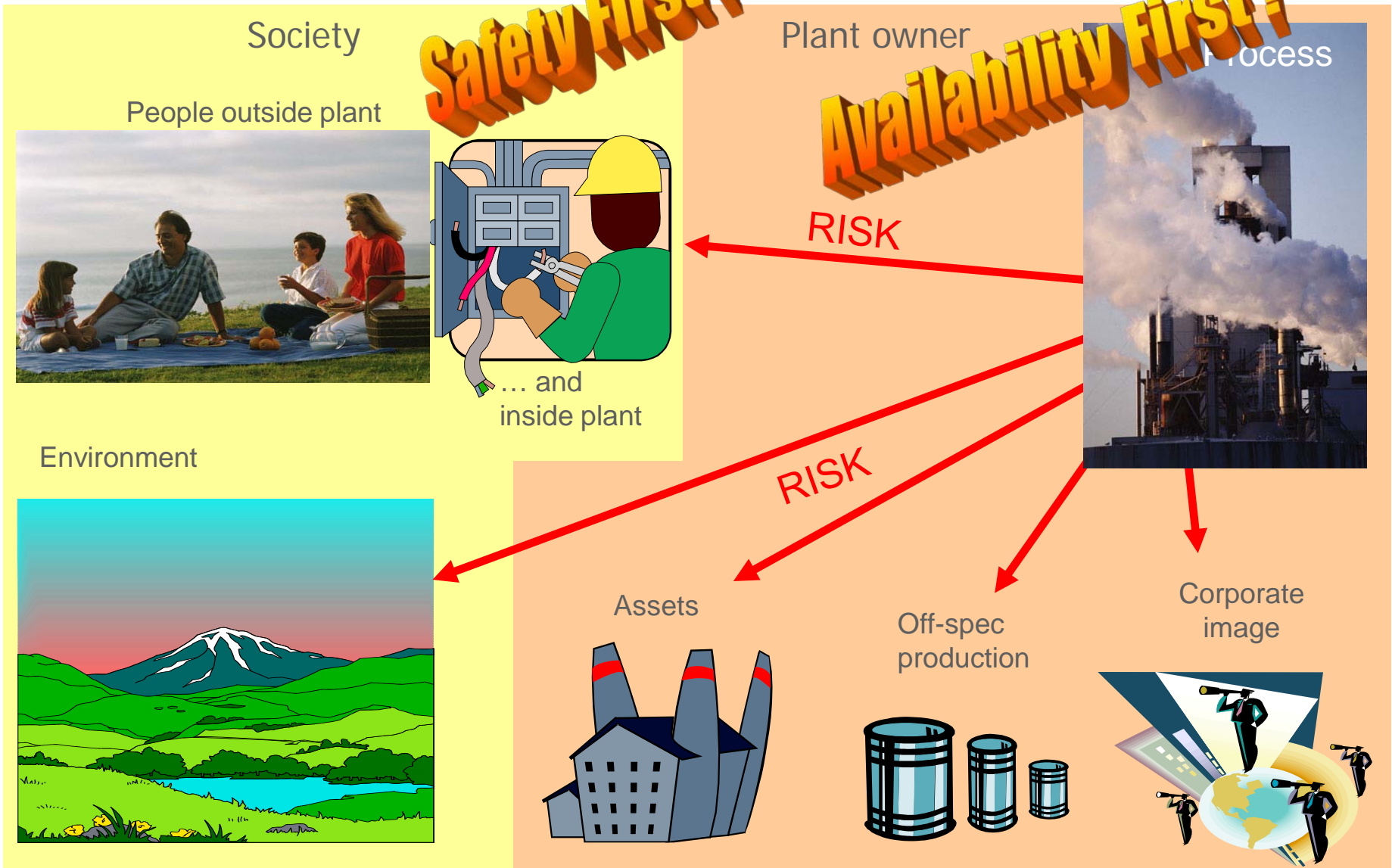
Consequences

(how serious, how much money, how many injuries, how many fatalities)

Demand Rate

(frequency, how many times per how many year)

What has to be Protected ?



Chemical Industry Accidents - History

Some of the major ones...

- 1974: Flixborough
- 1976: Seveso
- 1984: Bhopal
- 1988: Piper Alpha

And many more...

- 2010: BP Gulf of Mexico

the Consequences...

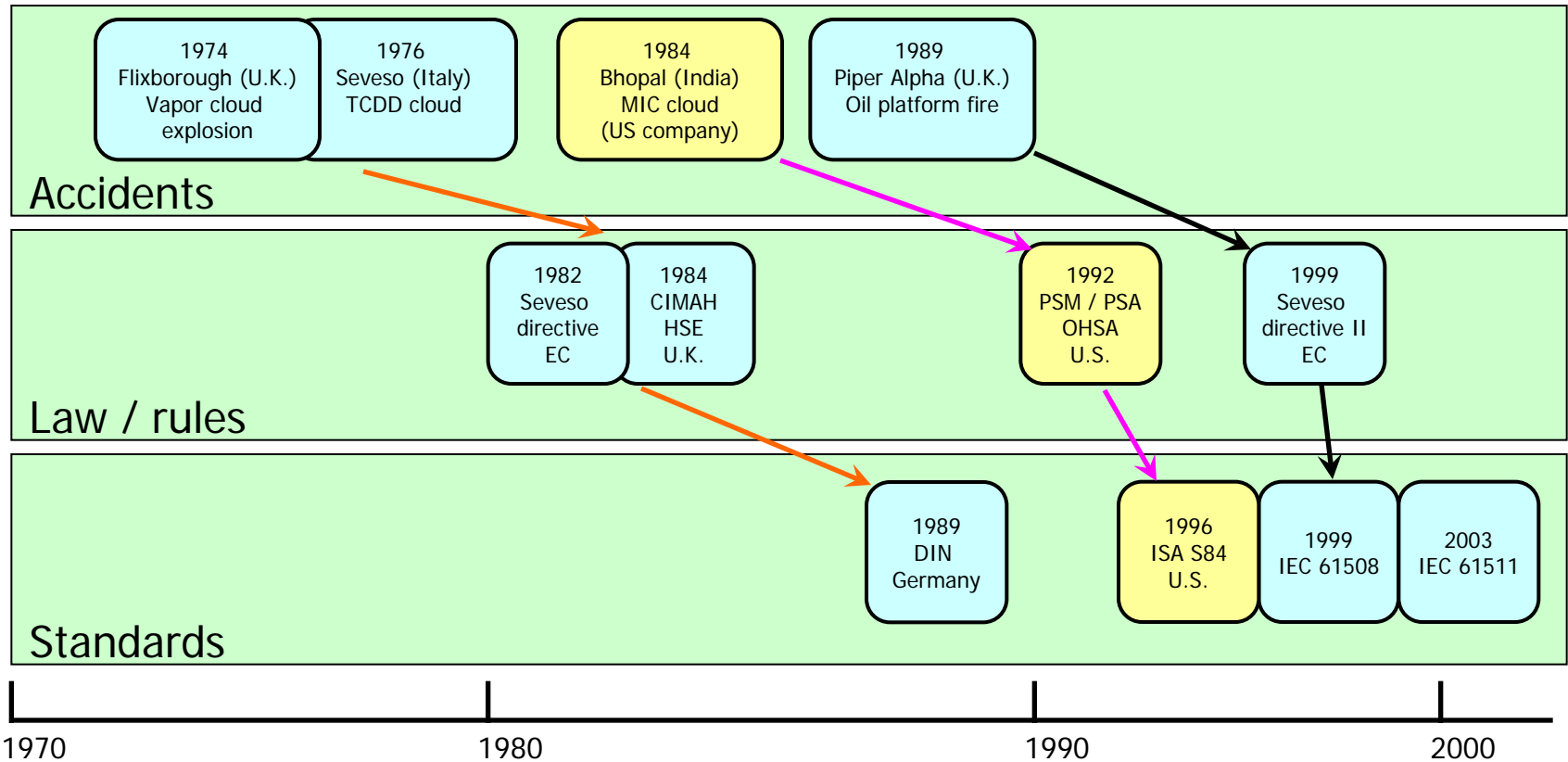
❖ Piper Alpha platform, July 1988



- 61 survivors, but many badly burnt
- 167 fatalities
- Piper Alpha was producing about 125,000 bpd in 1988
- Insured losses of over US\$ 3.4 Billion

Evolution of Regulations and Standards

History of Functional Safety Standards



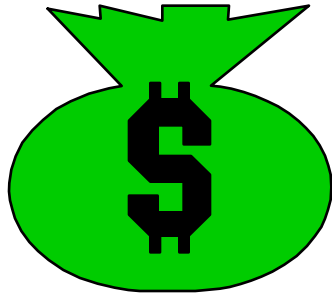
Preventing Accidents: Risk Reduction

RISK Assessment

Def. Risk

“Combination of the frequency of occurrence of harm and the severity of that harm”

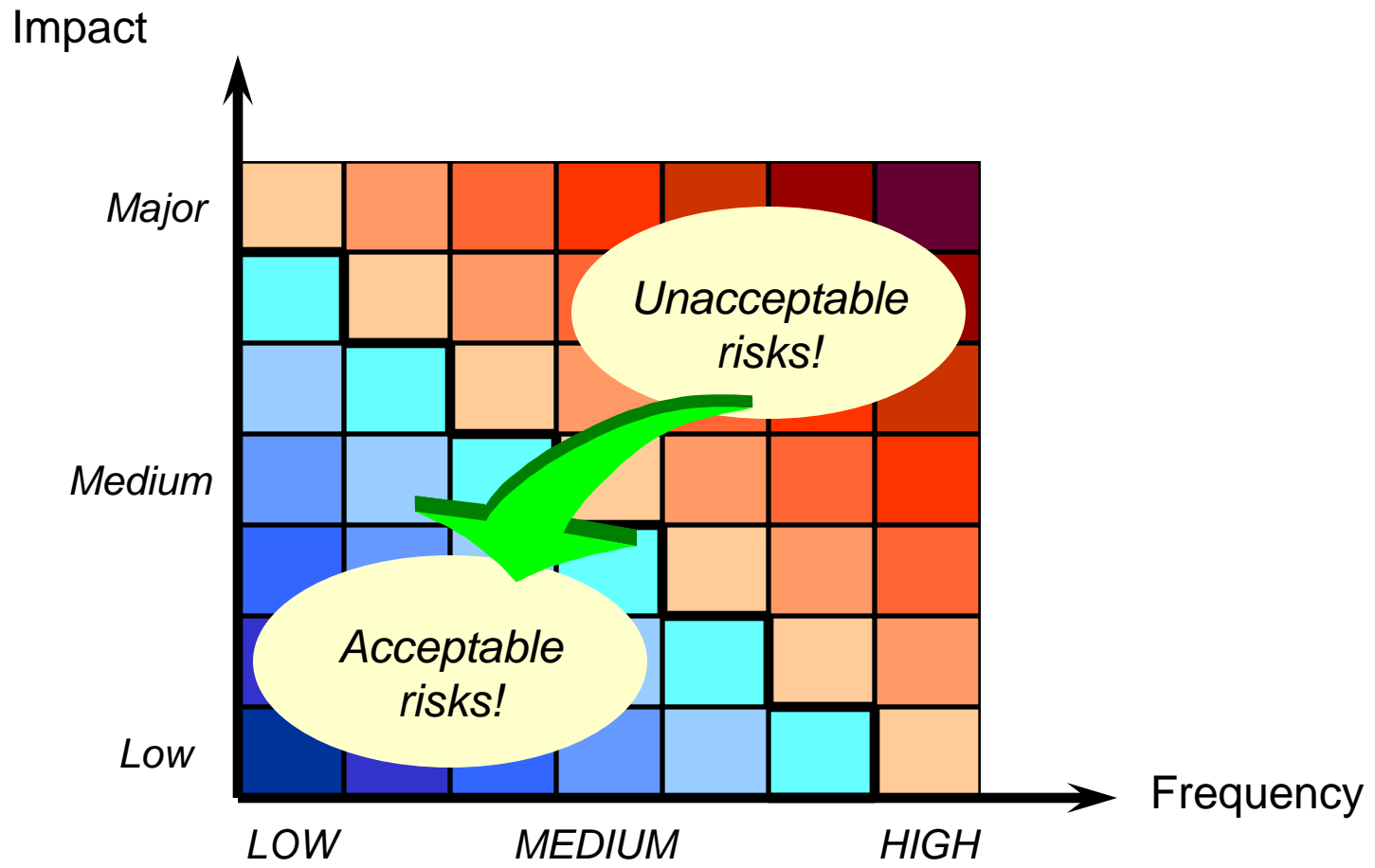
(IEC 61508 / IEC 61511)

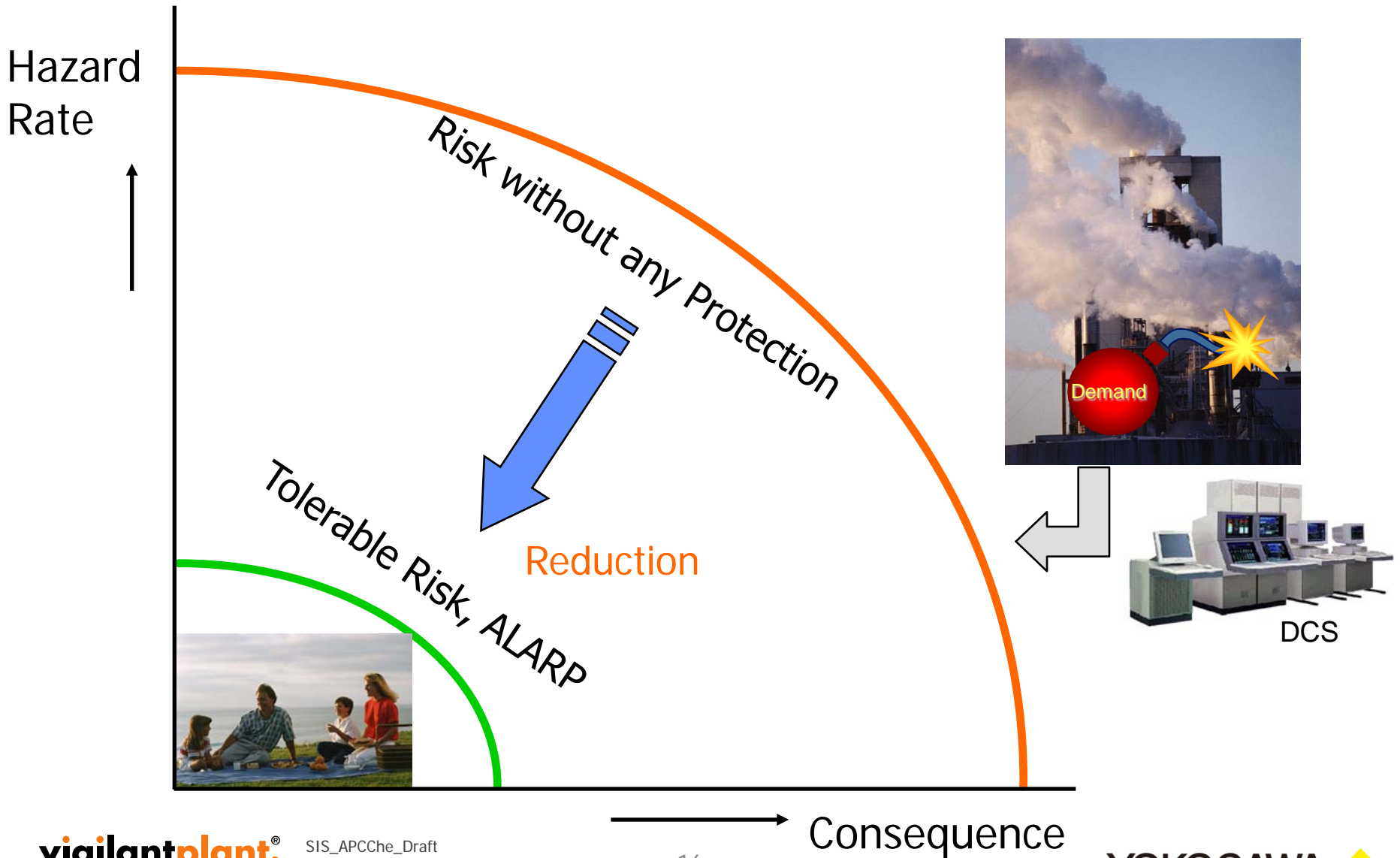


Risk = Impact X Frequency

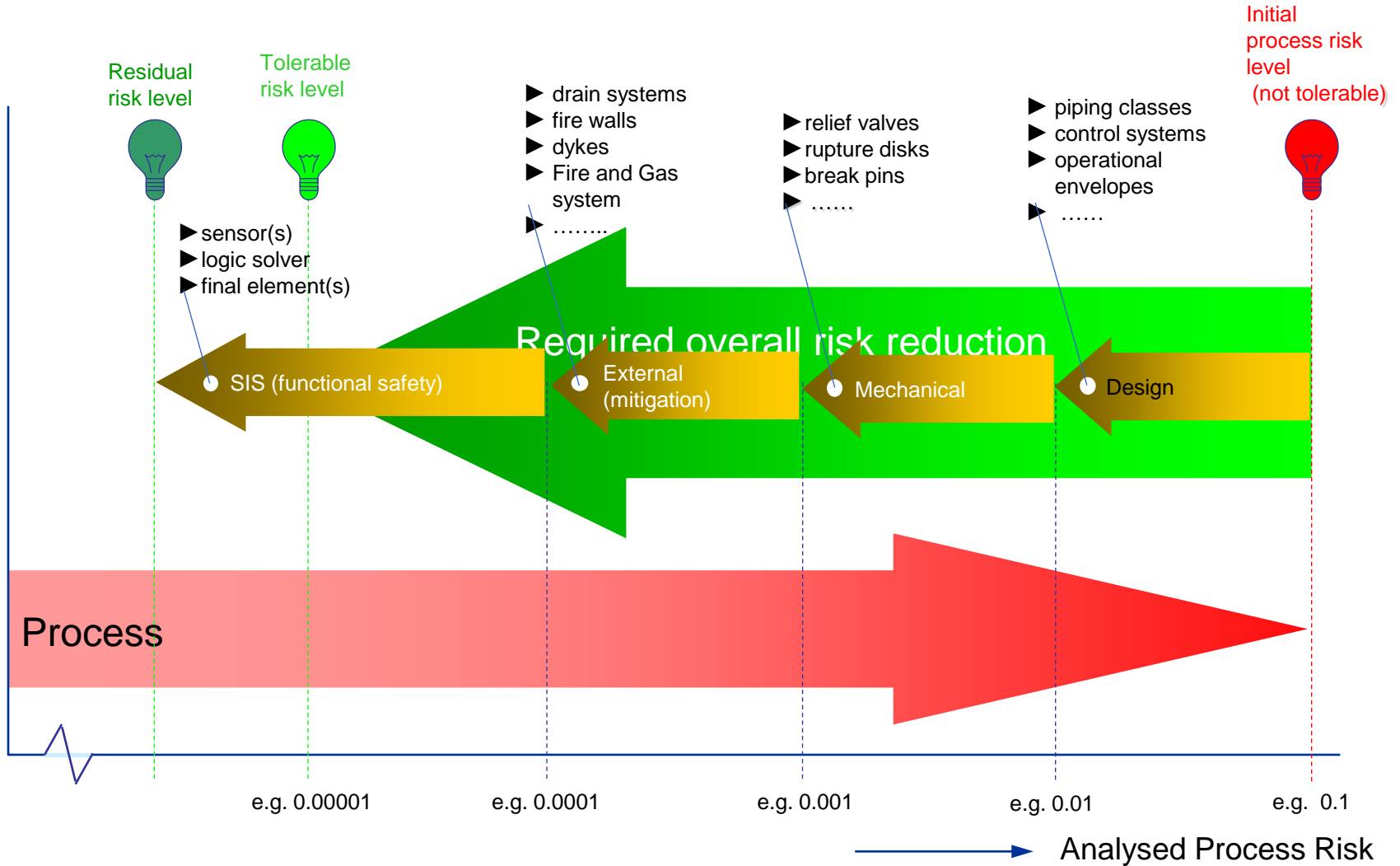
Impact = \$\$, Life, Environment

How to reduce the Risk?

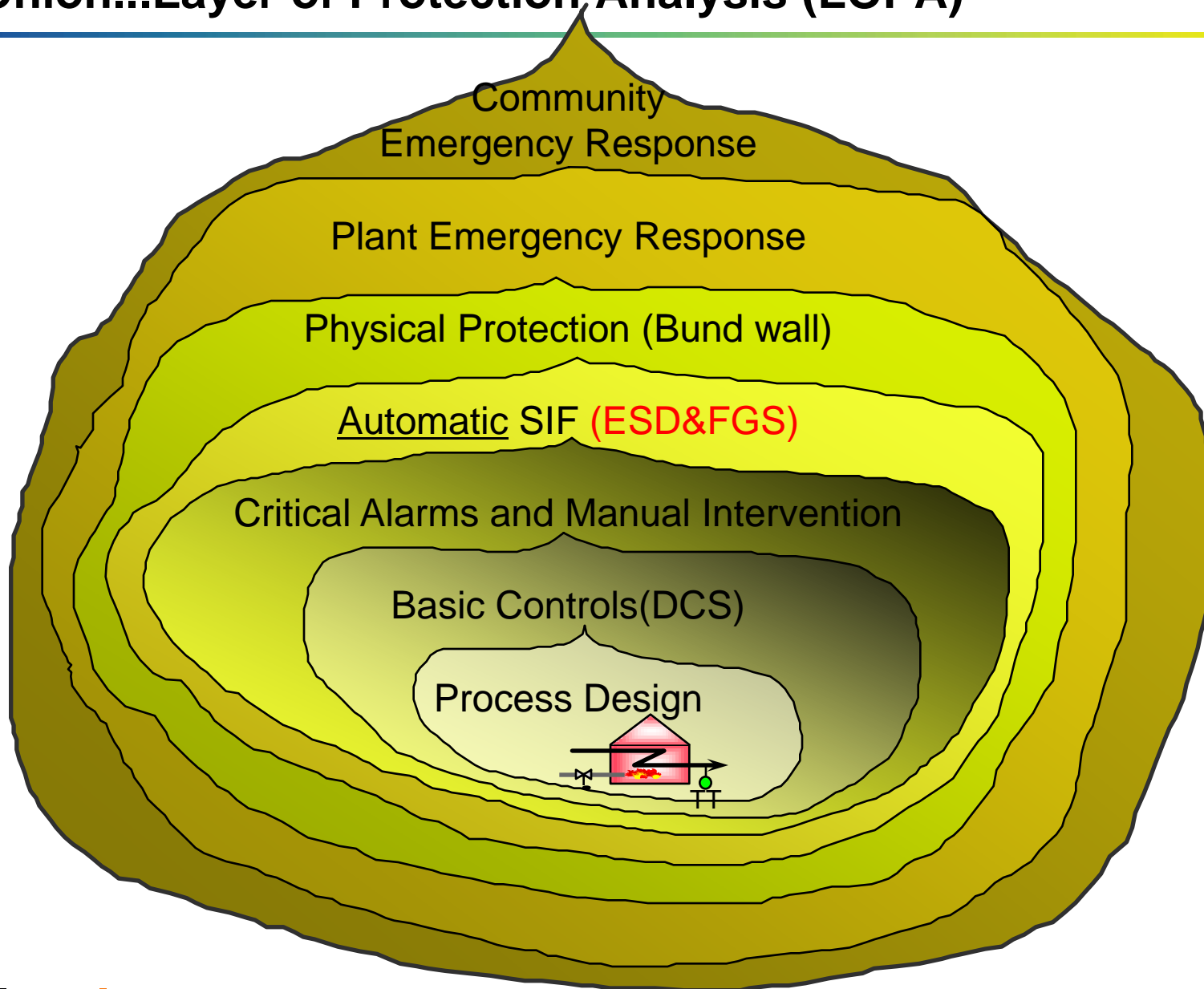




Process risk



Onion...Layer of Protection Analysis (LOPA)



❖ Case Study: Reliability of Instrumentation :
BP AMOCO Texas City Refinery:
Isomerization Unit Explosion, March 2005

BP AMOCO EXPLOSION MARCH '05



15 DEAD

100 INJURED

30 PUBLIC INJURED

8 IN CRITICAL CONDITION



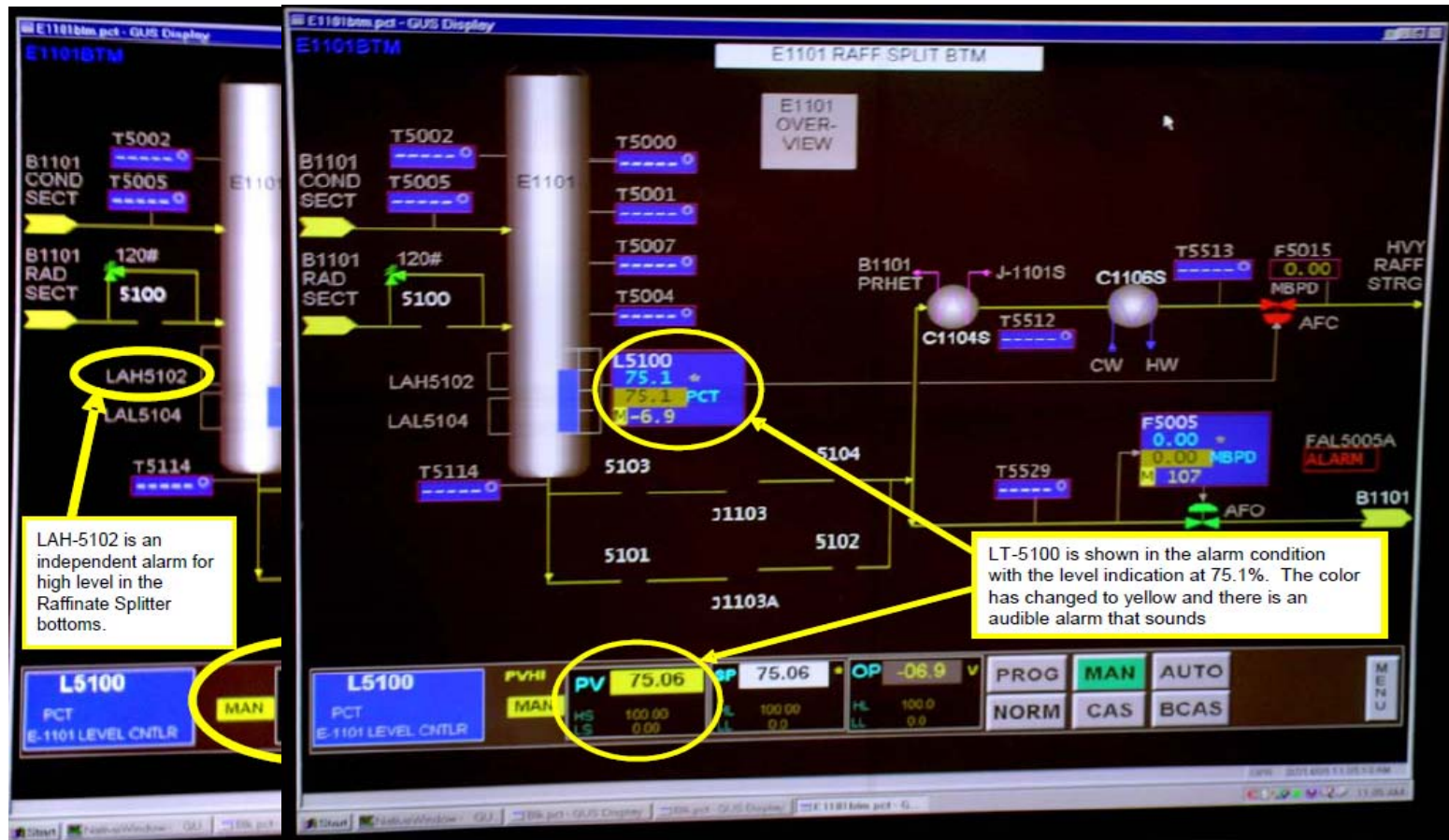
Gulf Freeway

at TCT Railroad South

An aerial photograph showing a large-scale oil spill cleanup operation in the ocean. Several long, parallel containment booms are visible, stretching across the water. The booms are supported by numerous small, yellow buoys. The water appears dark, and there are some white foam patches, likely from the cleanup process. The overall scene is a complex of industrial equipment in a natural marine environment.

The total cost of this incident for BP :
over \$US 2 Billion

❖ Failure of Raffinate Splitter Level Instrumentation



❖ DCS Level High Alarm was ignored

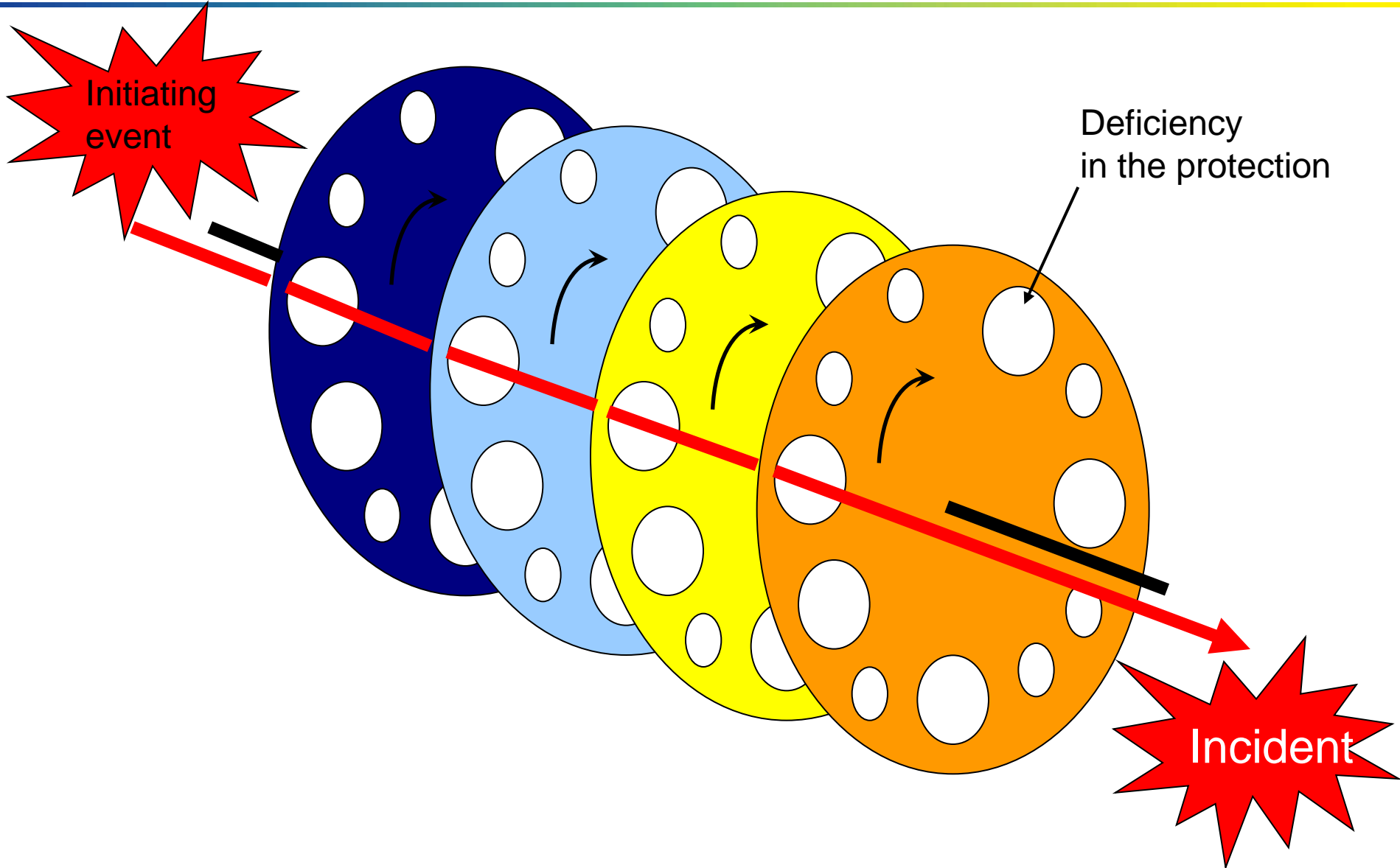
❖ Independent Level switch connected to alarm system did not work

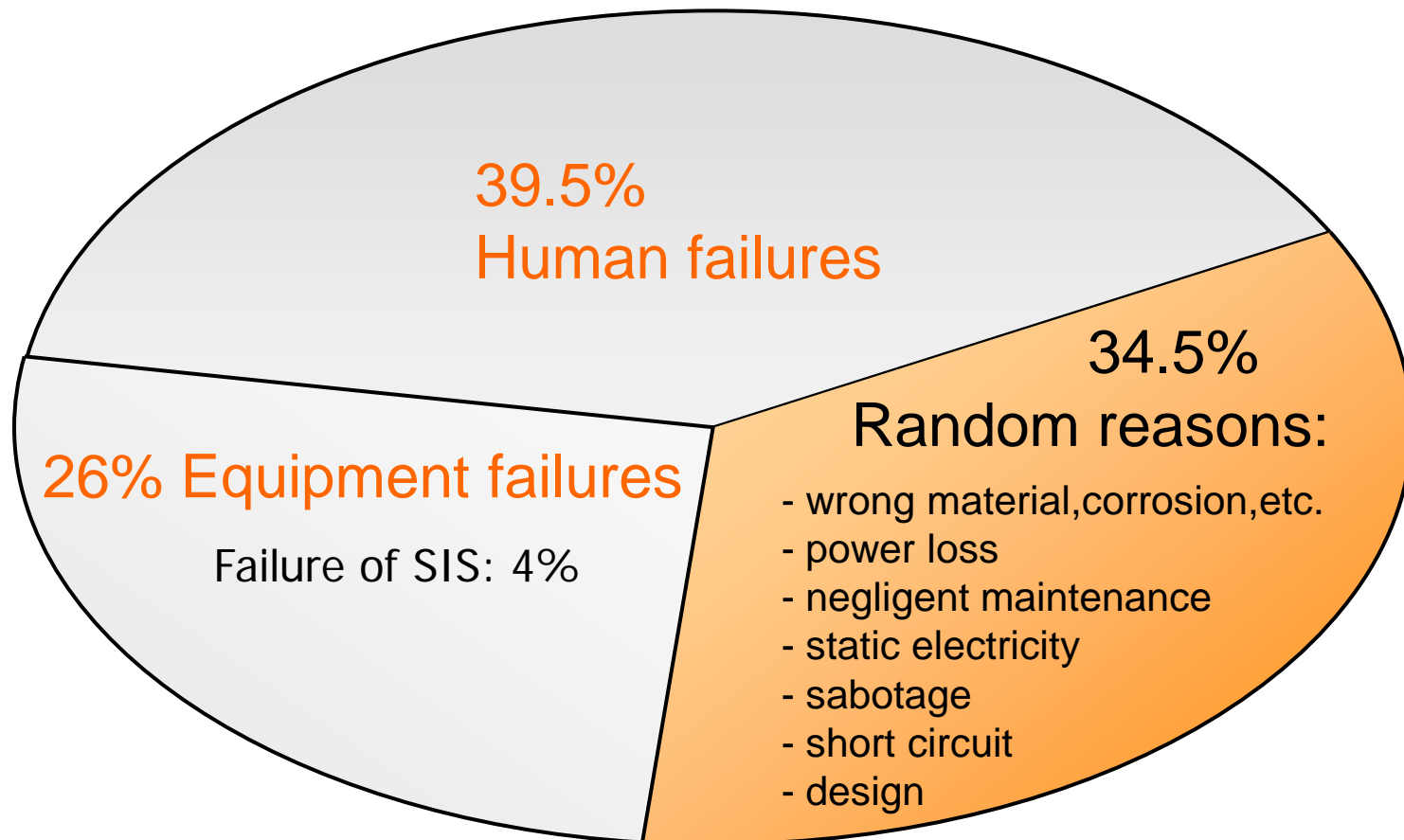
Source: Fatal Accident investigation Report :

http://www.bp.com/liveassets/bp_internet/us/bp_us_english/STAGING/local_assets/downloads/t/final_report.pdf

Accidents and Causes: The Human Factor

Layers of protection

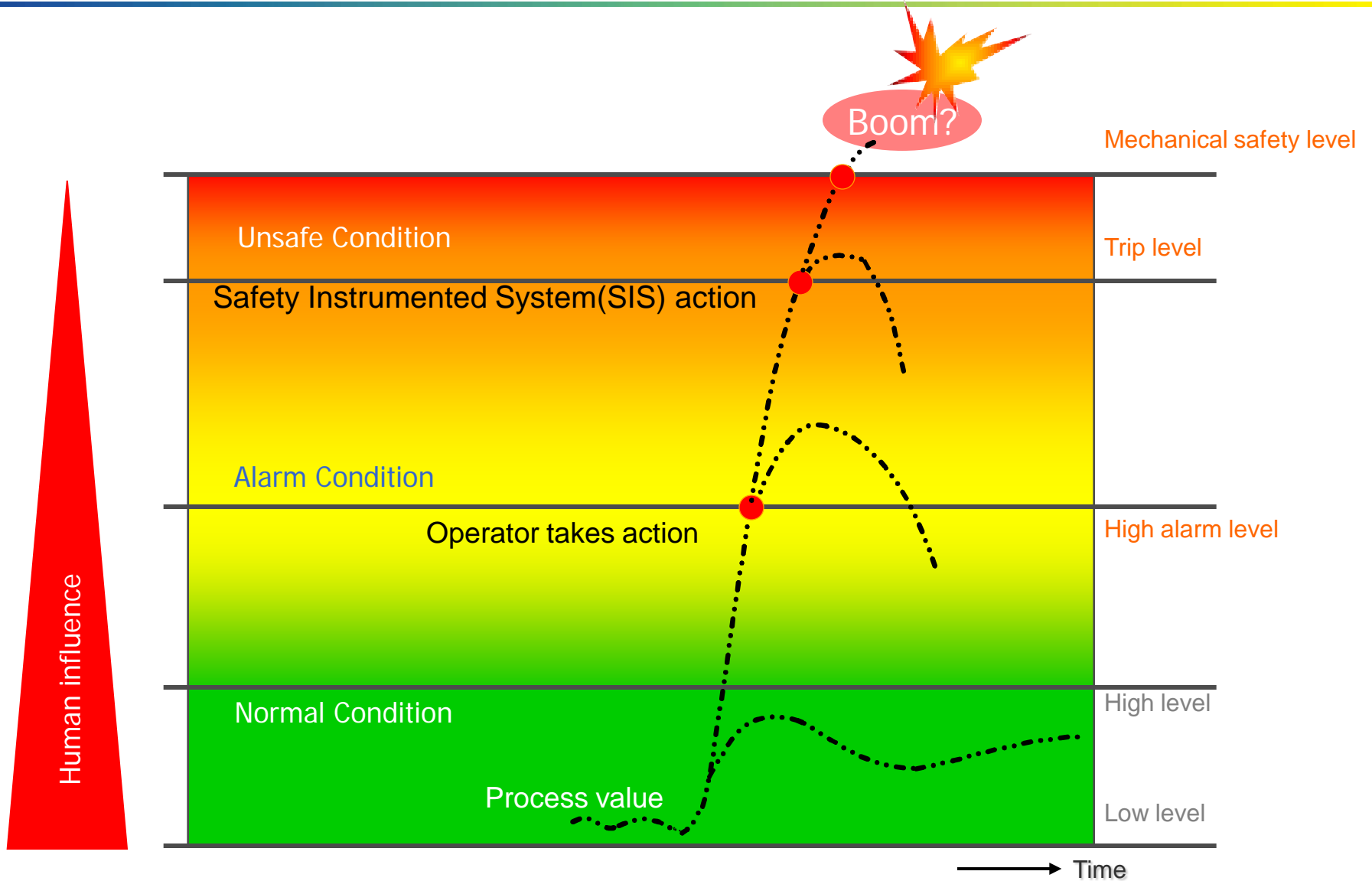




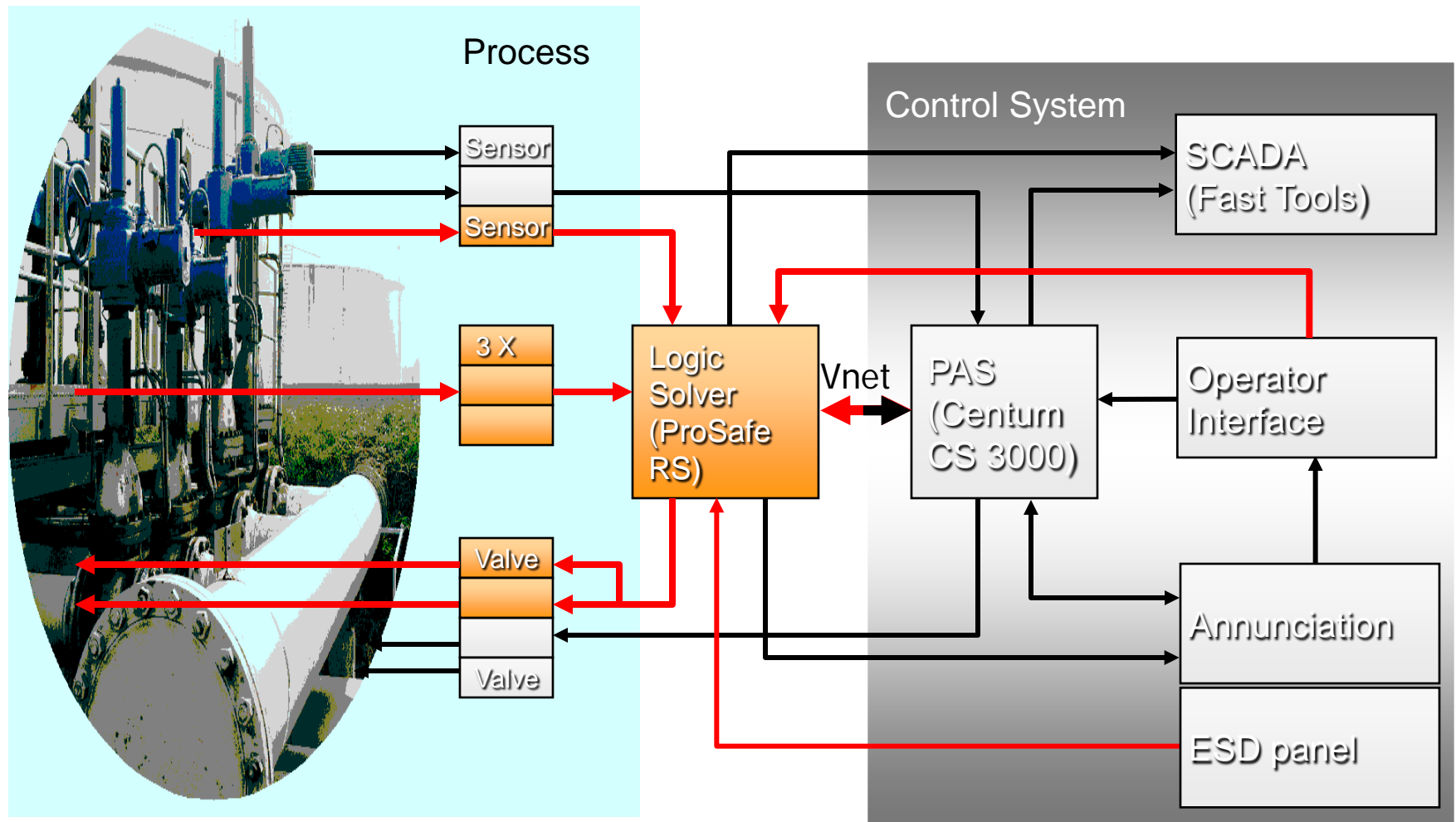
source: TNO investigations of 216 accidents

❖ Safety Instrumented Systems as a Safety Barrier

SIS Function in the Process



••• The position of SIS



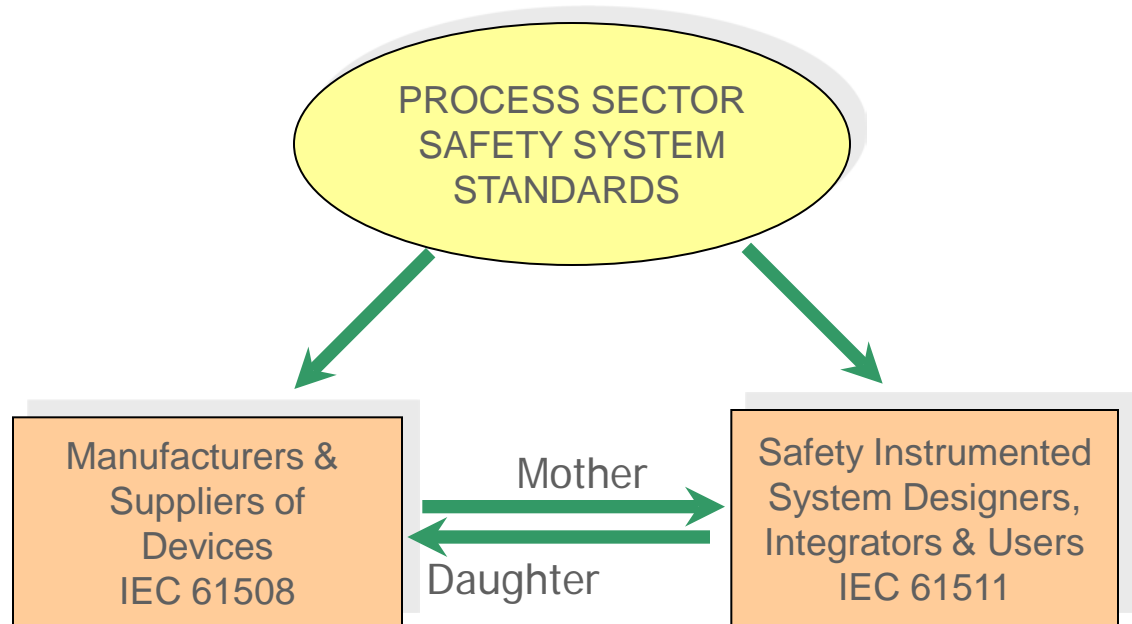
↔ = Safety related

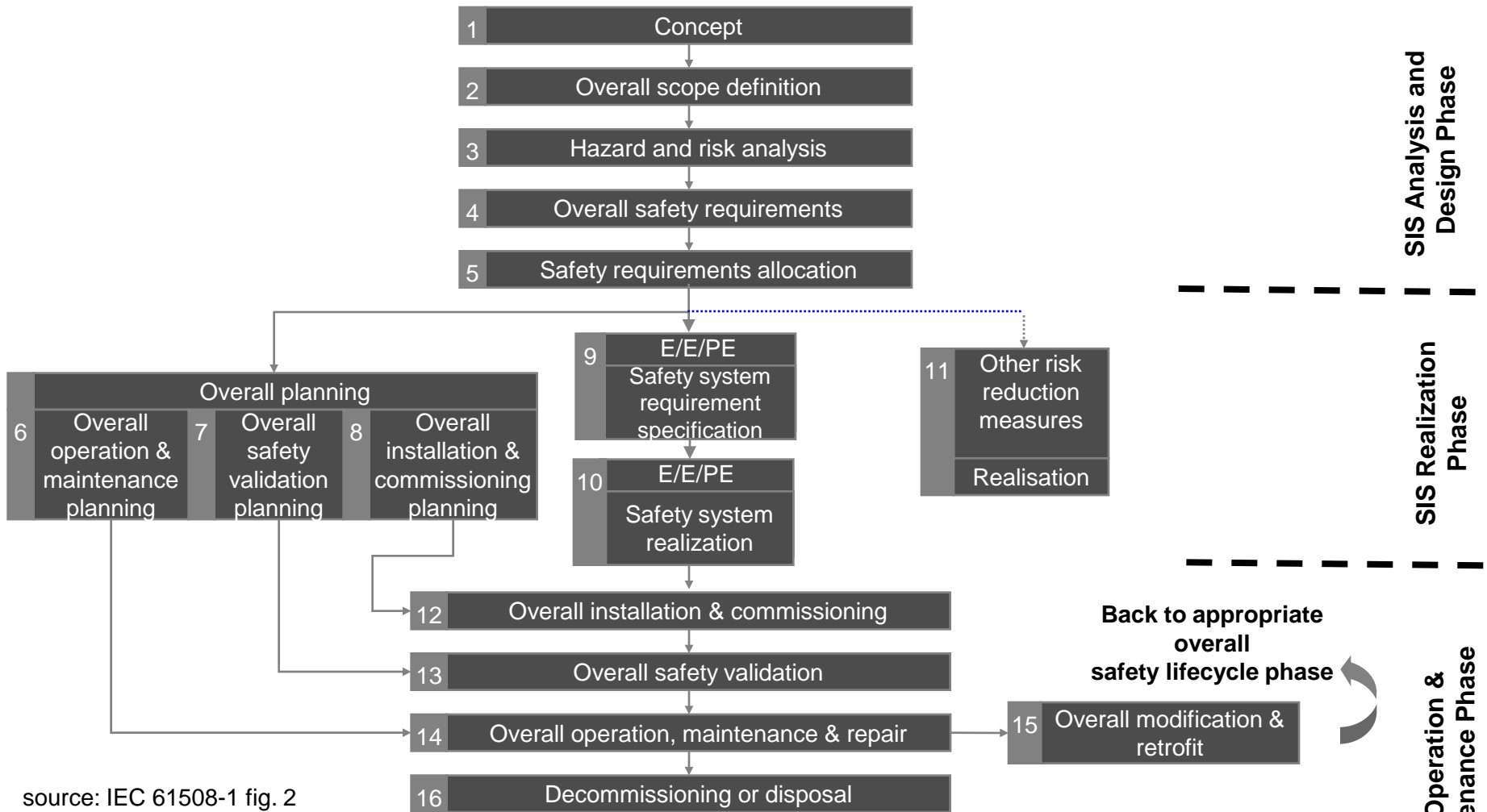
❖ Design & Engineering SIS: IEC 61508/ 61511 & FSM

The IEC 61508 / 61511 Standard

IEC 61508 : functional safety of electrical / electronic / programmable electronic safety-related systems.

IEC 61511 : functional safety for the process industry = identical to ISA-84.00.01 (except for grandfather clause)

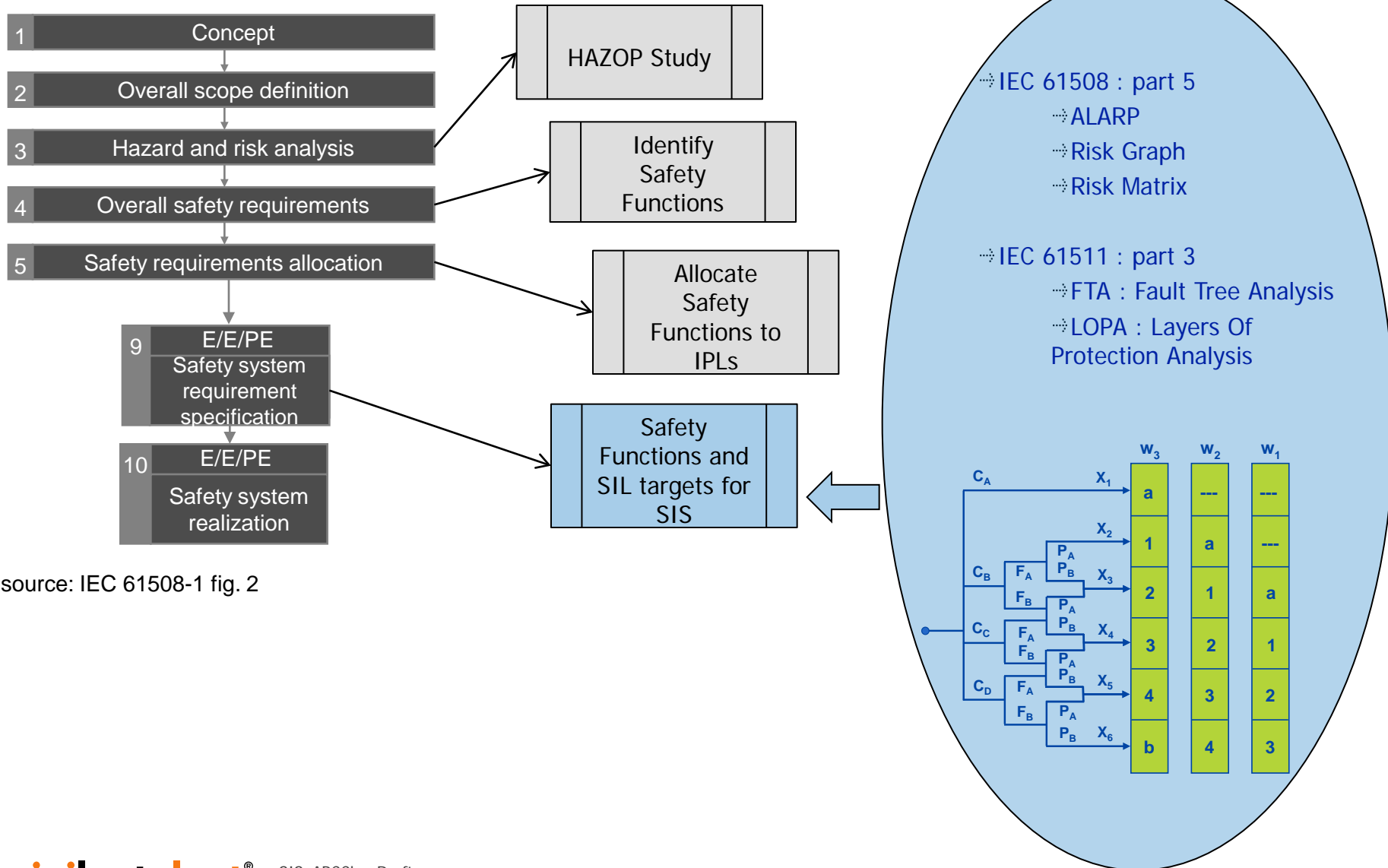




source: IEC 61508-1 fig. 2

 SIS: Analysis and Design phase

Hazard and Risk Analysis, SIL Allocation



source: IEC 61508-1 fig. 2

 SIS: Realization Phase

Safety Integrity Level

Three basic requirements have to be fulfilled in order to claim any SIL:

1. Hardware fault tolerance for the claimed SIL to be justified.
2. PFD_{AVG} (of all elements within a SIF) shall be within the claimed SIL bandwidth

Hardware Safety Integrity

3. Systematic Capability shall comply with the requirements for the claimed SIL

Systematic Safety Integrity

Hardware Safety Integrity: SIL Classification & PFD

Safety Integrity Level	Risk Reduction Factor (RRF)	Average Probability of failure on demand (PFD)
4	> 10 000	$\geq 10^{-5}$ to $< 10^{-4}$
3	1 000 - 10 000	$\geq 10^{-4}$ to $< 10^{-3}$
2	100 - 1 000	$\geq 10^{-3}$ to $< 10^{-2}$
1	10 - 100	$\geq 10^{-2}$ to $< 10^{-1}$
0	(No Safety Requirements)	

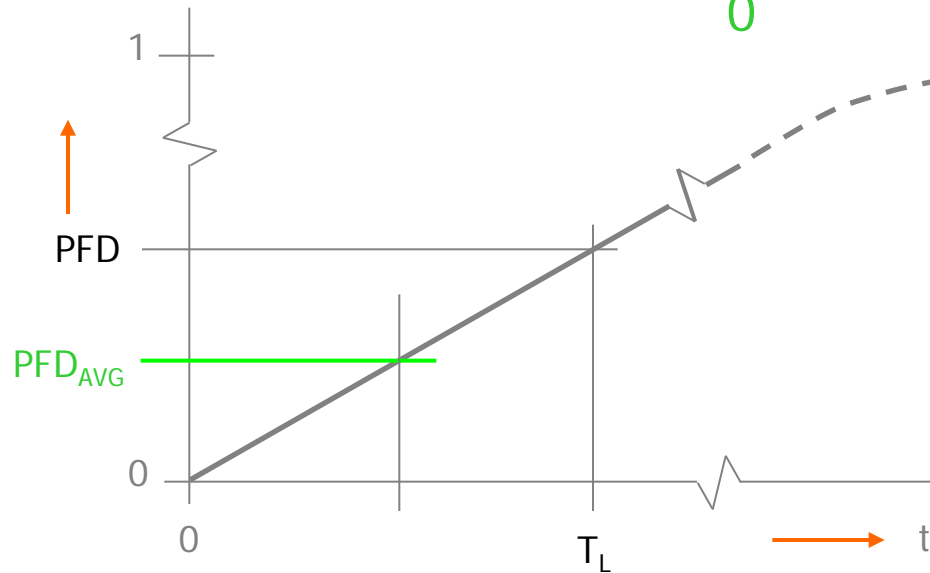
For Low Demand rate (less than once per year)

IEC 61508-1,
table 2

PFD : Probability of a Failure on Demand, derived from the safety parameters of the equipment.

$$PFD = 1 - e^{-\lambda_{Du} t}$$

$$PFD_{AVG} = \frac{1}{T_L} \int_0^{T_L} PFD(t) dt$$

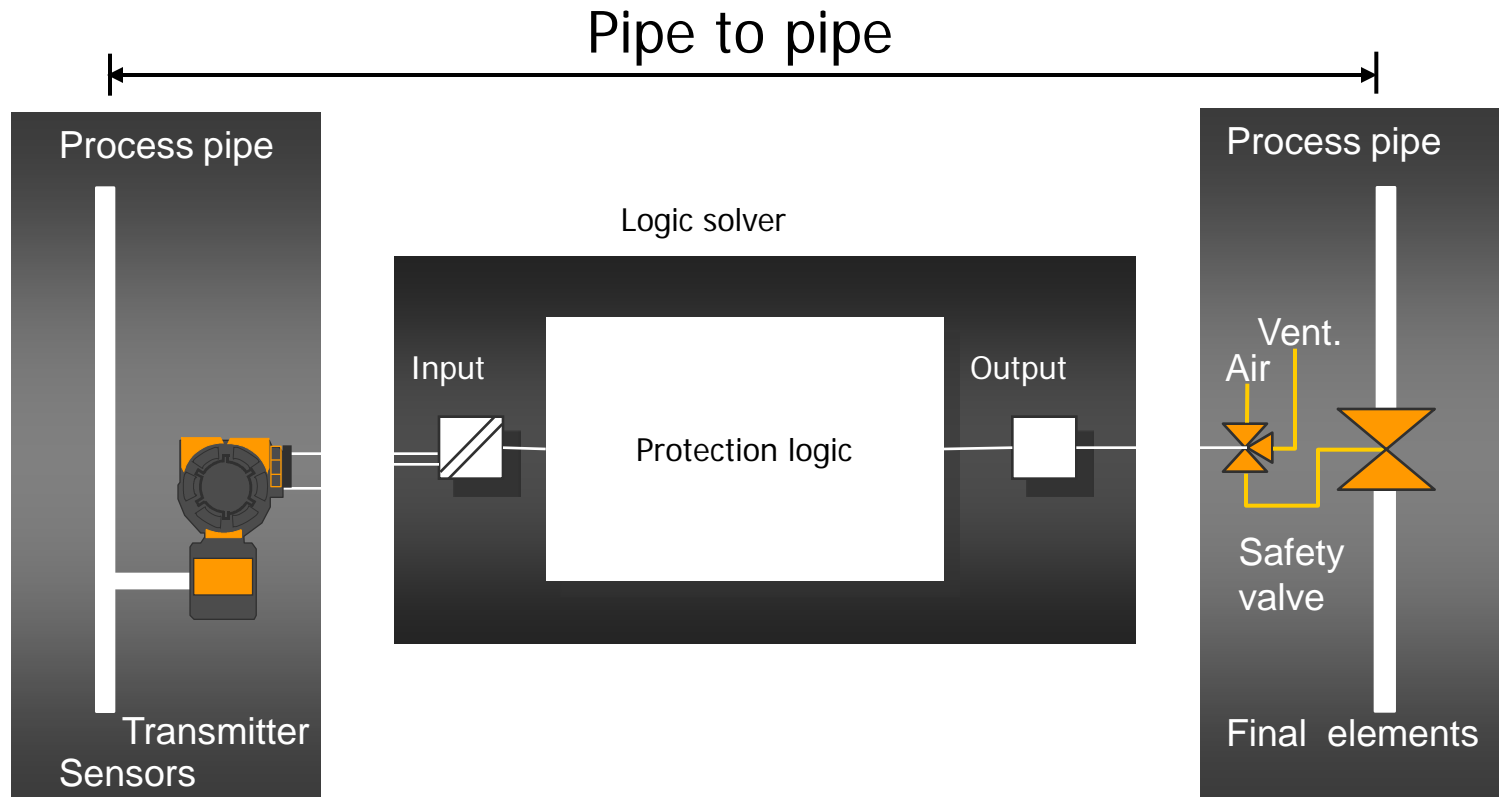


(T_L = life time)

$$PFD = \lambda_{Du} \times t$$

$$PFD_{AVG} = \frac{1}{2} \times \lambda_{Du} \times T_L$$

Hardware Safety Integrity: Average PFD for SIF

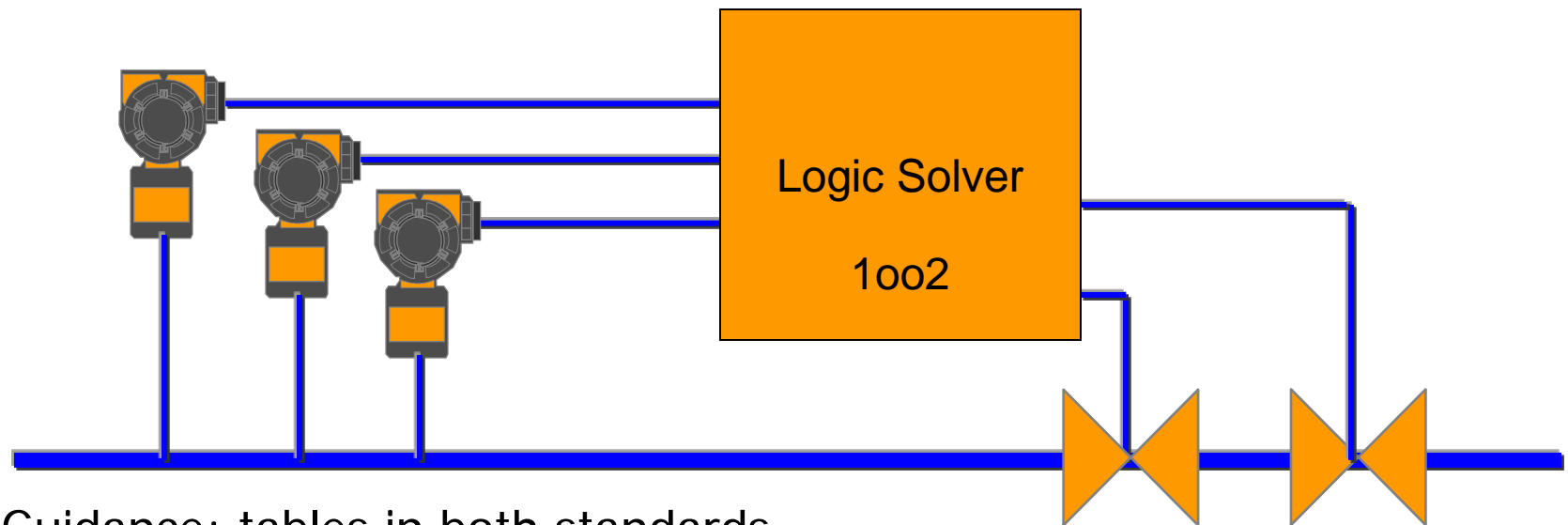


SIL \rightarrow PFD_{avg} (target) for the SIF

$$\text{PFD}_{\text{avg}} (\text{SIF}) = \text{PFD}_{\text{avg}} (\text{sensors}) + \text{PFD}_{\text{avg}} (\text{logic solver}) + \text{PFD}_{\text{avg}} (\text{final elements})$$

❖ Hardware fault tolerance

- ❖ The target SIL indicates the maximum PFDAVG but also depending on type and quality of the used device double / triple voting devices (1oo2, 1oo3) might be required



❖ Fault tolerance acc. IEC 61508-2

Table 2 — Hardware safety integrity: architectural constraints on type A safety-related subsystems

Safe failure fraction	Hardware fault tolerance (see note 2)		
	0	1	2
< 60 %	SIL1	SIL2	SIL3
60 % - < 90 %	SIL2	SIL3	SIL4
90 % - < 99 %	SIL3	SIL4	SIL4
> 99 %	SIL3	SIL4	SIL4

NOTE 1 See 7.4.3.1.1 to 7.4.3.1.4 for details on interpreting this table.

NOTE 2 A hardware fault tolerance of N means that N+1 faults could cause a loss of the safety function.

NOTE 3 See annex C for details of how to calculate safe failure fraction.

Table 3 — Hardware safety integrity: architectural constraints on type B safety-related subsystems

Safe failure fraction	Hardware fault tolerance (see note 2)		
	0	1	2
< 60 %	not allowed	SIL1	SIL2
60 % - < 90 %	SIL1	SIL2	SIL3
90 % - < 99 %	SIL2	SIL3	SIL4
> 99 %	SIL3	SIL4	SIL4

NOTE 1 See 7.4.3.1.1 to 7.4.3.1.4 for details on interpreting this table.

NOTE 2 A hardware fault tolerance of N means that N+1 faults could cause a loss of the safety function.

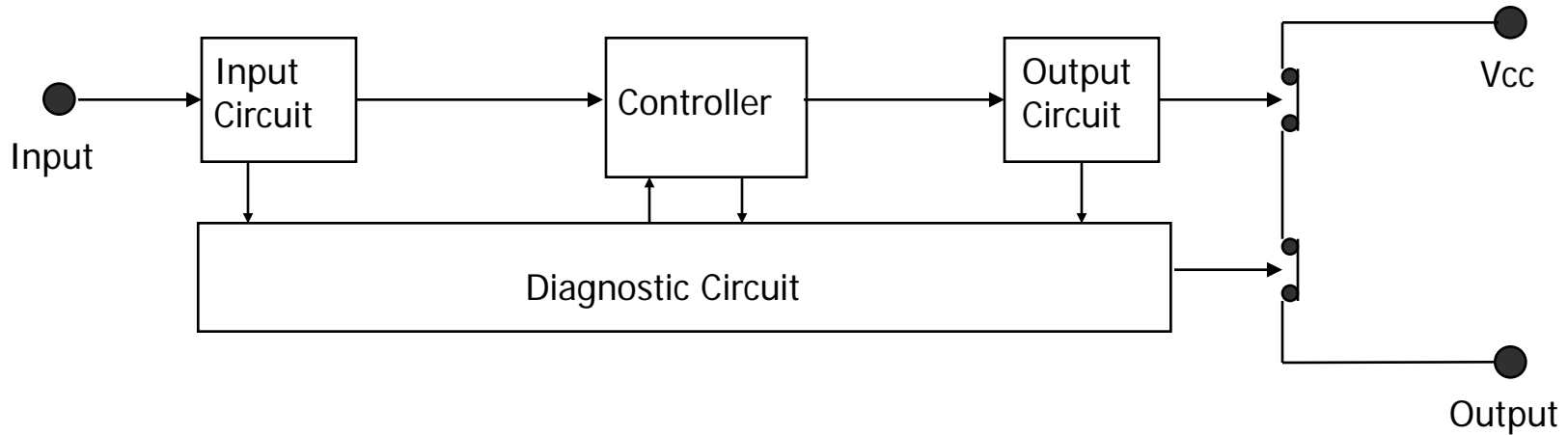
NOTE 3 See annex C for details of how to calculate safe failure fraction.

Type A : simple devices where the failure modes can easily be understood (mechanical devices, simple electronic devices like zener barrier, isolator etc.)

Type B : everything that is not simple, not type A.

❖ Logic Solver: Fault Tolerant Architecture

❖ 1001D architecture

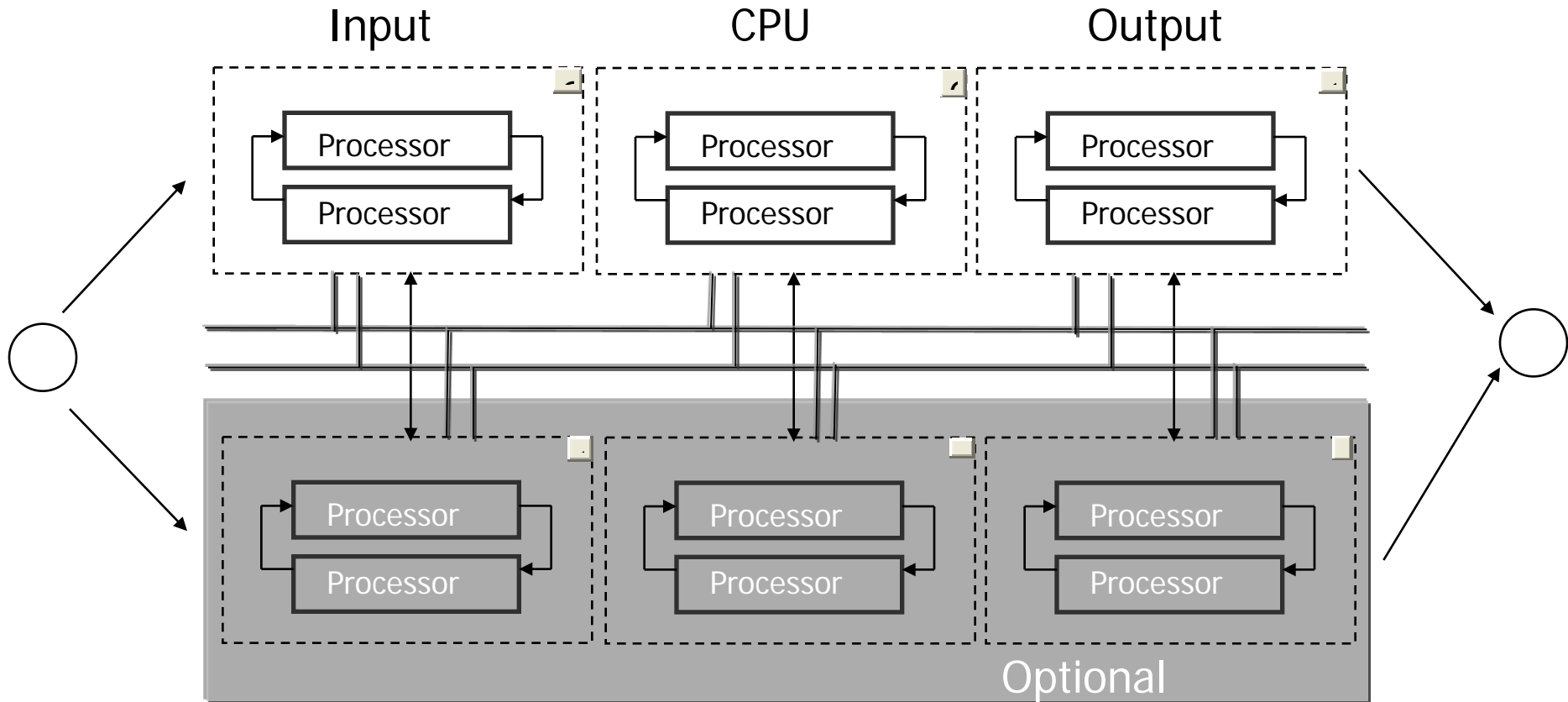


❖ Other popular Architectures include:

❖ 1002D

❖ 2003

❖ VMR 1001D



❖ Single SIL3 with high SFF

❖ Redundant configuration for High Availability

Measures to avoid systematic failures

- Employment of safety competent personnel
- Controlled realization
- Verification processes
- Configuration management
- Document control (including software)
- Functional Safety Assessment
- Validation processes
- Controlled operation, proof testing and maintenance
- Controlled site modifications

**Functional
Safety
Management
System as per
IEC
61508/61511**

❖ Responsibility of: End-user, Contractor, SIS equipment suppliers/ integrators

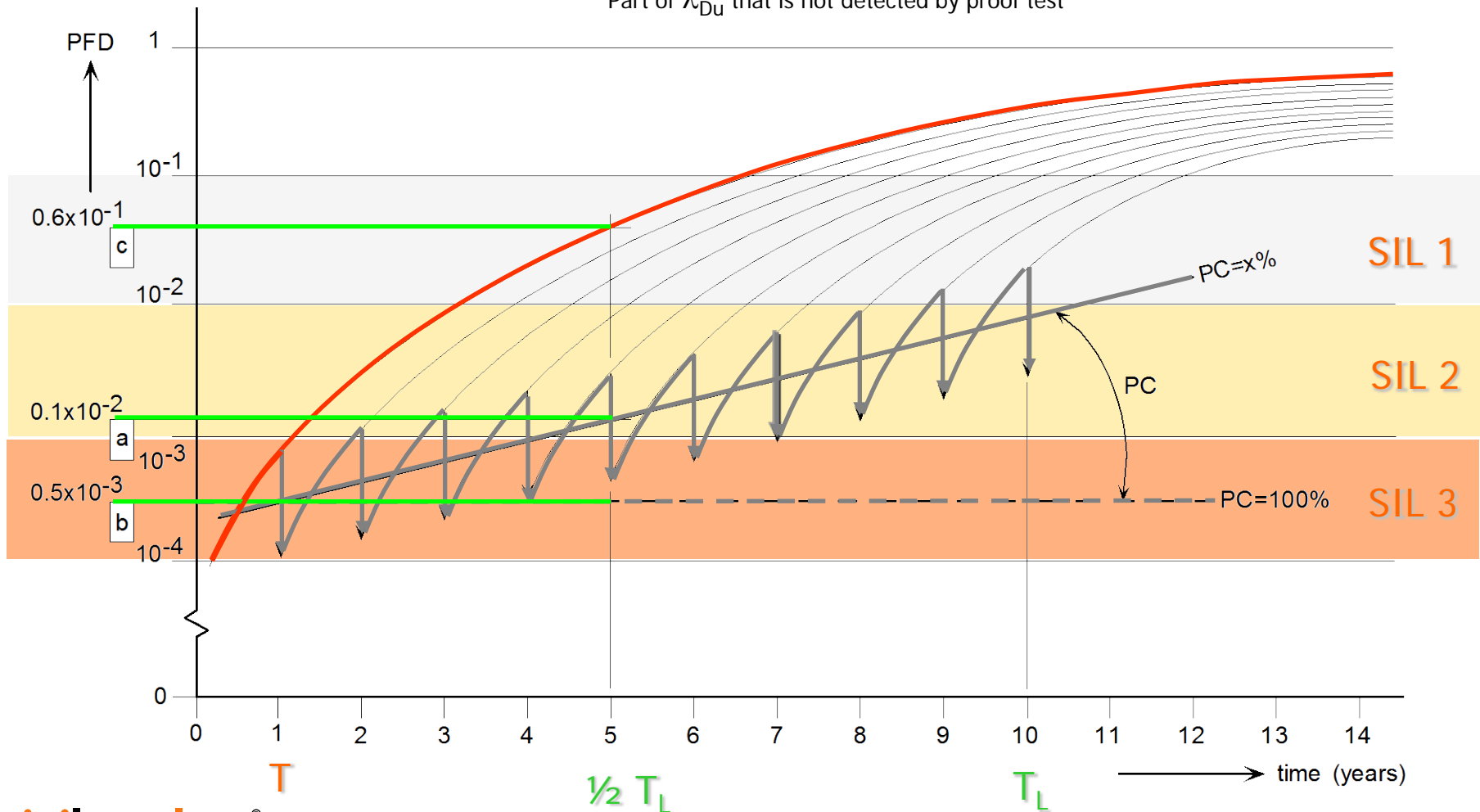
- ❖ SIS: Operation and Maintenance phase
 - Proof Testing
 - Management of Change

- ❖ A proof test means a complete test of the SIF, “pipe to pipe”.
- ❖ The purpose of the test is to reveal all “dangerous undetected” failures that are present in the SIF
- ❖ After the proof test the elements in the SIF should be in their initial state
- ❖ Proof Test Coverage: The proof test of the system does not completely restore the initial state due to:
 - Imperfect testing
 - Imperfect repair
 - Ageing

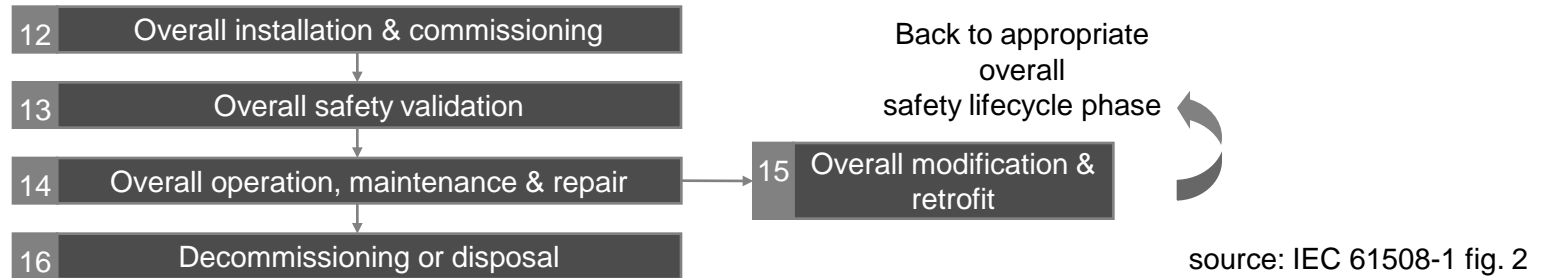
Impact of Proof testing on PFD_{AVG}

Without proof test $\rightarrow PFD = 1 - e^{-\lambda_{Du} t}$ Or approximated as, $PFD = \lambda_{Du} \times t$ and $PFD_{AVG} = \frac{1}{2} \times \lambda_{Du} \times T_L$

With proof test $\rightarrow PFD_{AVG} = \frac{1}{2} \times PC \times \lambda_{Du} \times T + \frac{1}{2} \times (1 - PC) \times \lambda_{Du} \times T_L$
 Part of λ_{Du} that is not detected by proof test



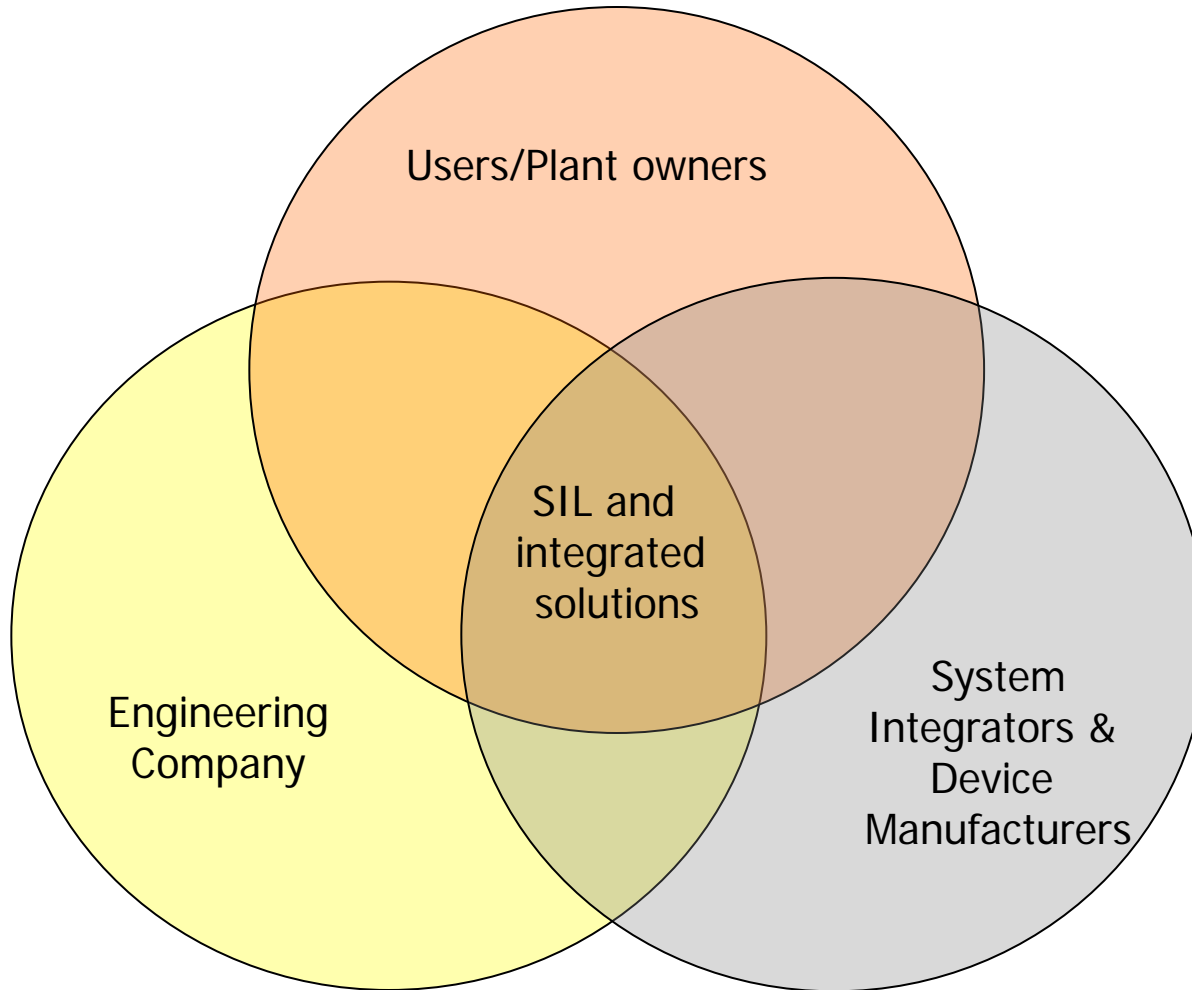
❖ Management of Change



❖ Prior to modifying the SIS functions on a running installation, a hazard and risk analysis needs to be carried out >> Management of Change procedure

Functional Safety Management

- Who should have a documented and auditable functional safety management system?





**Functional
Safety
Management
System in
accordance
with IEC
61508/ 61511**



Thanks For Your Kind Attention!